

For I.G.
 $h = h(T)$ only &
 $u = u(T)$ only

22-141 50 SHEETS
 22-142 100 SHEETS
 22-144 200 SHEETS



$$v = \frac{V}{m} \text{ m}^3/\text{kg} \quad w = w_{\text{m}} \quad v_f = v_f + x v_{fg}$$

$$v \approx v_f @ T \text{ (in compressed region)} \quad u \approx u_f @ T \text{ (compressed region)} \quad h = h_f + v_f (P - P_{\text{sat}}) @ T \text{ (compressed region)}$$

$$x = \frac{m_{\text{vap}}}{m_{\text{tot}}} \quad v = \frac{v_{\text{tot}}}{m_{\text{tot}}} \quad v_f = \frac{v_{fg}}{m_{fg}} \quad v_g = \frac{v_{\text{vap}}}{m_{\text{vap}}}$$

$$h = u + Pv \quad h = u + RT \text{ (I.G., rev.)} \quad 1-x = \frac{m_{\text{liq}}}{m_{\text{tot}}} \quad x v_g = \frac{v_{\text{vap}}}{m_{\text{tot}}}$$

$$u_2 - u_1 = \int C_v dT \text{ (} u = u(T) \text{ only)}$$

$$h_2 - h_1 = \int C_p dT \text{ (} h = h(T) \text{ only)}$$

$$Pv = nRT \text{ (I.G., rev.)} \quad R = \frac{R}{m}$$

$$Pv = mRT \text{ (I.G., rev.)}$$

$$Pv = RT = \text{const. (I.G., rev.)} \quad M = \frac{m}{n}$$

$$\frac{P_1 v_1}{T_1} = \frac{P_2 v_2}{T_2} \text{ (I.G., Rev.)}$$

$$C_p - C_v = R \quad C_p = \frac{kR}{k-1}$$

$$k = \frac{C_p}{C_v} \quad C_v = \frac{R}{k-1}$$

$Pv^n = \text{const.} = \text{polytropic process}$
 $n=0 \Rightarrow P = \text{const.}$
 $n=1 \Rightarrow T = \text{const.}$
 $n=k \Rightarrow s = \text{const.}$
 $n \rightarrow \infty \Rightarrow v = \text{const.}$

$Pv^k = \text{const.}$ (Isentropic, I.G.)
 $C_p = \text{const.}$

$$\frac{P_1}{P_2} = \left(\frac{v_2}{v_1}\right)^k \quad \left(\frac{P_2}{P_1}\right)^{\frac{1}{k}} = \frac{v_2}{v_1}$$

$$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{\frac{k-1}{k}} \quad \left(\frac{T_2}{T_1}\right)^{\frac{k}{k-1}} = \frac{P_2}{P_1}$$

($\Delta s = 0, \text{ I.G.}$)
 ($C_p = \text{const.}$)

Throttling process implies $h_1 = h_2$ (adiabatic)

$$s_2 - s_1 = C_v \ln \frac{T_2}{T_1} + R \ln \frac{v_2}{v_1} \quad \left. \begin{array}{l} \text{I.G.} \\ C_p = \text{const.} \end{array} \right\}$$

$$s_2 - s_1 = C_p \ln \frac{T_2}{T_1} - R \ln \frac{P_2}{P_1}$$

$$\Delta s = \int C_p \frac{dT}{T} - R \ln \frac{P_2}{P_1} \text{ (I.G.)} \quad \rightarrow = s_2^* - s_1^*$$

$$\frac{P_1}{T} + \frac{\bar{v}_1^2}{2} + g z_1 = \frac{P_2}{T} + \frac{\bar{v}_2^2}{2} + g z_2 \text{ (Rev., S.F., } w_{\text{to}} = 0 \text{)}$$

$$w = -v(P_2 - P_1) \text{ (Rev., } \Delta KE \approx 0, v = \text{const.)}$$

$$w = -v(P_2 - P_1) \text{ (S.F., } \Delta PE \approx 0 \text{ (Pump))}$$

$$\eta_{\text{TH}} = \frac{w_{\text{net}}}{Q_H} = \frac{Q_H - Q_L}{Q_H} = 1 - \frac{Q_L}{Q_H} \text{ (heat engine)} \quad \eta_{\text{TH}} = 1 - \frac{T_L}{T_H} \text{ (Carnot H.E.)}$$

$$\text{COP}_C = \beta = \frac{Q_L}{w_{\text{net}}} = \frac{Q_L}{Q_H - Q_L} = \frac{Q_L}{T_H - T_L} \text{ (Carnot)}$$

$$\text{COP}_H = \gamma = \frac{Q_H}{w_{\text{net}}} = \frac{Q_H}{Q_H - Q_L} \quad 1 < \gamma < \infty$$

$$\gamma - \beta = 1$$

$$w = \int P dv \text{ (closed system, reversible)}$$

$$w = P(v_2 - v_1) \text{ (closed sys., Rev., } P = \text{const.)}$$

$$w = \frac{P_2 v_2 - P_1 v_1}{1-n} \text{ (closed system, Rev., } T \neq \text{const., I.G.)}$$

$$w = P_1 v_1 \ln \left(\frac{v_2}{v_1}\right) = RT \ln \left(\frac{P_1}{P_2}\right) \text{ (closed sys. Rev., } T = \text{const. I.G.)}$$

$$q - w = u_2 - u_1 \text{ (closed system, } \Delta KE \approx 0, \Delta PE \approx 0)$$

$$\dot{Q} + \sum \dot{m}_i \left(h_i + \frac{\bar{v}_i^2}{2} + g z_i \right) = \dot{W} + \sum \dot{m}_e \left(h_e + \frac{\bar{v}_e^2}{2} + g z_e \right)$$

$$\frac{\dot{Q}}{\dot{m}} = q \quad \dot{m} = \rho \vec{V} A = \frac{\vec{V} A}{v} \quad P = \frac{P}{RT} \quad \frac{\dot{W}}{\dot{m}} = w$$

$$q - w = h_2 - h_1 \text{ (S.F., } \Delta KE \approx 0, \Delta PE \approx 0)$$

$$w = P v \ln \frac{v_2}{v_1} = RT \ln \frac{P_1}{P_2} \text{ (} P v^n = \text{const., } T = \text{const., I.G.)}$$

$$w = n \left(\frac{P_2 v_2 - P_1 v_1}{1-n} \right) \text{ (} n \neq 1, \text{ I.G., } P v^n = \text{const.)}$$

$$w = \frac{kR(T_2 - T_1)}{1-k} = C_p(T_1 - T_2) \text{ (} n = k, \Delta s = 0 \text{)}$$

$$q = \int T ds \text{ (reversible)}$$

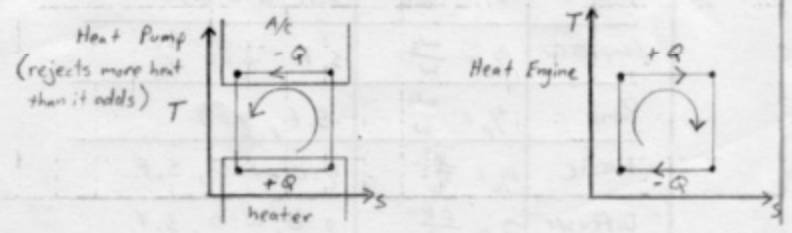
$$T ds = du + P dv \text{ (pure simple compressible subst.)}$$

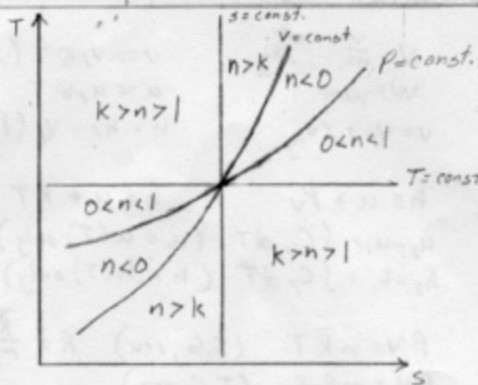
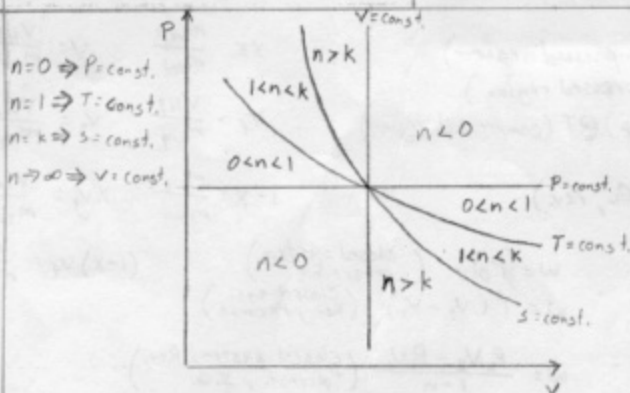
$$T ds = dH - v dP$$

$$T ds = dU + P dv$$

$$w = - \left\{ v dP - \frac{\bar{v}_2^2 - \bar{v}_1^2}{2} - g(z_2 - z_1) \right\} \text{ (Rev., S.F.)}$$

$$w = - \int v dP \text{ (Rev., } \Delta KE \approx 0, \Delta PE \approx 0)$$





$n=0 \Rightarrow P = \text{const.}$
 $n=1 \Rightarrow T = \text{const.}$
 $n=k \Rightarrow s = \text{const.}$
 $n \rightarrow \infty \Rightarrow v = \text{const.}$

- Isothermal $\Rightarrow T = \text{const.}$
- Isobaric $\Rightarrow P = \text{const.}$
- Adiabatic $\Rightarrow q = 0$
- Polytropic $\Rightarrow Pv^n = \text{const.}$ (I.G., $c_p = \text{const.}$)
- Isentropic $\Rightarrow \Delta s = 0$ (reversible, adiabatic)
- c_p = pressure specific heat
- c_v = volume specific heat
- q = heat transfer
- u = internal energy
- h = enthalpy
- M = molecular weight
- n = # kmols / # lbmols
- s = entropy
- \bar{s} = s per mole

- Turbines
 - Compressors
 - Pumps
 - Nozzles
 - Diffusers
- } Isentropic

$^{\circ}R = ^{\circ}F + 459.67$

$^{\circ}K = ^{\circ}C + 273.15$

$$\bar{R} = \begin{cases} 8.314 \text{ kJ/kmol}\cdot\text{K} \\ 1.986 \text{ BTU/lbmol}\cdot^{\circ}R \\ 1545 \text{ ft}\cdot\text{lb}/\text{lbmol}\cdot^{\circ}R \end{cases}$$

$$\left(\frac{\text{ft}^2}{\text{s}^2}\right) = \left(\frac{\text{ft}^2}{\text{s}^2}\right) \left(\frac{1 \text{ BTU}}{778 \text{ ft}\cdot\text{lb}}\right) \left(\frac{1 \text{ lb}}{32.2 \text{ lbm}}\right) = \frac{\text{BTU}}{\text{lbm}} = \left(\frac{\text{BTU}}{\text{lb}}\right) \left(\frac{32.2 \text{ lbm}}{\text{ft}^2/\text{s}^2}\right) \left(\frac{778 \text{ ft}\cdot\text{lb}}{\text{BTU}}\right) = \frac{\text{ft}^2}{\text{s}^2}$$

$$\left(\frac{\text{m}^2}{\text{s}^2}\right) = \left(\frac{\text{m}^2}{\text{s}^2}\right) \left(\frac{1 \text{ kJ}}{1 \text{ kg}\cdot\text{m}^2/\text{s}^2}\right) \left(\frac{1 \text{ J}}{1 \text{ N}\cdot\text{m}}\right) = \text{J/kg} \div 1000 = \text{kJ/kg}$$

$P_r = \frac{P}{P_{\text{crit.}}}$
 $T_r = \frac{T}{T_{\text{crit.}}}$
 $Pv = ZRT$

- w if outside does work on system
 if Q goes in its pos.
 if w leaves its pos.

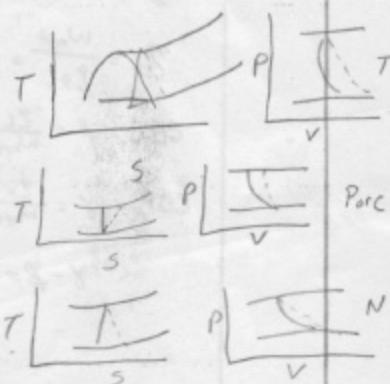
S.F. No change at a point w/ respect to time

Device	η_{th}	assumptions
Turbine	$\eta_T = \frac{w}{w_s}$	S.F., $Q=0$ (+) net work
Compressor	$\eta_C = \frac{w_s}{w}$	S.F., $q=0$
Pump	$\eta_P = \frac{w_s}{w}$	S.F., $q=0$
Nozzle	$\eta_N = \frac{V_2^2}{V_1^2}$	$q=0, w=0$, S.F.
Diffuser	$\eta_D = \frac{\Delta P}{\Delta P_s}$	$q=0, w=0$, S.F.

$\dot{V} = \dot{V}A$

$\frac{P_2}{P_1} = \left(\frac{P_2}{P_1}\right)_{\text{isentropic}}$

$\frac{V_2}{V_1} = \left(\frac{V_2}{V_1}\right)_{\text{isentropic}}$



$(m_2 - m_1)c_v + m_c - m_i = 0$ $Q + m_i(h_i + \frac{V_i^2}{2} + gz_i) = W + m_c(h_c + \frac{V_c^2}{2} + gz_c) + m_2(u_2 + \frac{V_2^2}{2} + gz_2) - m_1(u_1 + \frac{V_1^2}{2} + gz_1)$ U.S.U.F